

# Magnetic sugarcane bagasse composite for atrazine and fluoride removal

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## Abstract

**BACKGROUND:** The present investigation focuses on the synthesis and application of a magnetic adsorbent material formed by the agro-industrial waste sugarcane bagasse (SCB). Its application in the removal of fluoride and atrazine demonstrates its properties as a potential adsorbent material for the treatment of contaminated wastewater.

**RESULTS:** The synthesis method proved to be simple and reproducible. The presence and distribution of magnetite and fluoride on the surface of the material were studied by characterization techniques (SEM, EDX, FTIR-ATR). Several specific functional groups were identified which may interact with atrazine and fluoride molecules in the adsorption process. Kinetic results indicated that second- and pseudo-second-order model fitted better for the fluoride and atrazine adsorption processes, respectively. The adsorption processes took place by chemisorption onto heterogeneous surfaces. Isotherm data fitted better to the Langmuir–Freundlich model in both systems; therefore, the process took place by a combination of mechanisms. Cellulose and lignin from sugarcane bagasse contribute in the adsorption process, while magnetite not only improve performance of composite for the removal of the chemical species tested, but also achieve a simple separation process via magnetic interactions' with a common magnet. The adsorption capacities of the composites were 0.5036 mg g<sup>-1</sup> for fluoride and 40.11 mg g<sup>-1</sup> for atrazine.

**CONCLUSION:** The synthesis of the magnetic composite is simple and generates a material that is easy to manipulate and isolate after the process. The affinity of the composite with atrazine is greater than with fluoride; however, the composite can be used in systems with low concentration.

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**Keywords:** magnetite nanoparticles; sugarcane bagasse; atrazine; fluoride

## INTRODUCTION

The three most common forms of iron oxides in nature are magnetite (Fe<sub>3</sub>O<sub>4</sub>), maghemite (γ-Fe<sub>2</sub>O<sub>3</sub>) and hematite (α-Fe<sub>2</sub>O<sub>3</sub>).<sup>1</sup> Magnetite is composed of Fe<sup>2+</sup>, Fe<sup>3+</sup> and O<sup>2-</sup> species packaged in an inverse spinel structure, where O<sup>2-</sup> ions forming a face-centered cubic lattice, and iron cations occupy interstitial sites.<sup>2</sup>

Magnetite is a magnetic mineral that can be found in nature<sup>3</sup> A synthetic form of magnetite can be produced by different simple methods with a high degree of purity.<sup>4</sup> These methods allow control of magnetite form and size. Nanoparticles of magnetite (MNP) with size <10–20 nm exhibit a form of superparamagnetism.<sup>1</sup> In the presence of a low external magnetic field, nanoparticles tend to exhibit a high magnetization response, which is gradually lost with distance from the magnetic field. This property is characteristic of superparamagnetic materials.<sup>5</sup> Some of the most relevant applications include (but are not limited to): magnetic recording, (photo) catalysis, pigments, ferrofluids, contrast agent for magnetic resonance imaging, drug delivery, adsorption support, anti-tumoral agent and bioseparation.<sup>6</sup> Although magnetite has been used as adsorbent material for fluoride removal,<sup>7</sup> and for other applications,<sup>8</sup> usually it is found as part of composites.<sup>9</sup> Magnetite composites have been used in biomedical applications,<sup>10</sup> catalysis,<sup>11</sup> removal of heavy metals,<sup>12,13</sup> pesticides,<sup>14</sup> and organic compounds,<sup>15,16</sup> and radioactive species.<sup>17</sup>

Lignocellulosic materials, such as those found in agro-industrial waste, have proven to be a good alternative as supports to obtain composite materials due to their abundance and low cost.<sup>14</sup> The use of waste materials obviously is attractive due to their contribution in reducing the costs of their disposal, therefore contributing to environmental protection.<sup>18</sup> Various agricultural wastes have been explored as low-cost adsorbents, including sugarcane bagasse (SCB).<sup>19</sup> This residue, in its natural form, has been shown to have capacity for removal of heavy metals,<sup>20</sup> halogens such as fluoride,<sup>21</sup> and organic molecules such as dyes.<sup>22</sup> A magnetic modified SCB was prepared by Yu *et al.*<sup>19</sup> to study its adsorption

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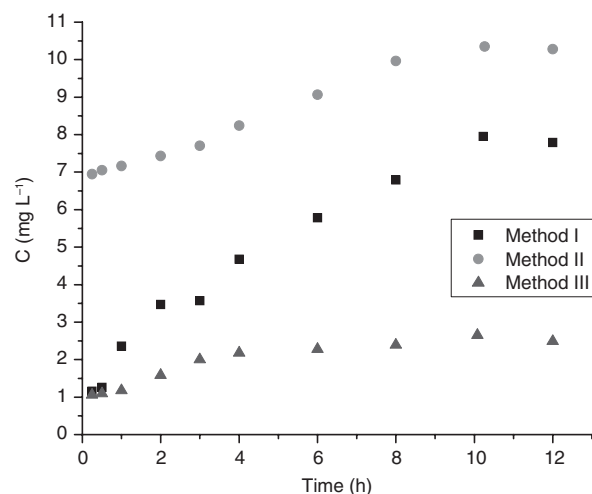
and desorption of  $Pb^{2+}$  and  $Cd^{2+}$ . Those experiments showed that the prepared magnetic sorbent had good adsorption performances for heavy metal ions, including high adsorption capacity and rapid adsorption rate. To the best of our knowledge, this kind of composite has not yet been applied to the removal from aqueous solutions of fluoride or atrazine, two pollutants that have been found to alter water quality, representing a risk for the aquatic environment and human health.

Fluoride was routinely added to drinking water because small concentrations of it could be helpful for teeth care. However, a high concentration can be dangerous to human health:<sup>23</sup> dental fluorosis is a sign that fluoride concentration, in the human body, has reached harmful levels.<sup>24</sup> Therefore, high concentrations of this halogen in water should be considered an alarming problem.

Some pesticides, including atrazine, are applied and marketed without any restriction in some countries.<sup>25</sup> Atrazine has been prohibited in Europe since 2010 due to its toxicity. However, it can still be found as noxious waste.<sup>26</sup> On the one hand, atrazine is associated with birth defects<sup>27</sup> and a significant increase in the prevalence of small-for-gestational-age (SGA) babies in humans.<sup>28</sup> On the other, it causes an oestrogenic effect in sexually mature female European quail<sup>29</sup> and is considered an endocrine disruptor on fish.<sup>30</sup>

Several techniques have been used for atrazine and fluoride removal, some of which can be expensive<sup>31</sup> or polluting.<sup>32</sup> Adsorption is an excellent alternative to be used for water decontamination processes since it is low-cost, ecofriendly and easy to implement from laboratory level to industrial scale. Therefore, many different kinds of materials and composites have been used as adsorption materials in processes for fluoride and atrazine removal. A laminated Yttrium-based nanocomposite with high surface area prepared for fluoride removal had an adsorption capacity calculated by the Langmuir isotherm model of  $31.0 \text{ mg g}^{-1}$ .<sup>33</sup> Chen *et al.*<sup>34</sup> prepared a novel tri-metal nanocomposite by a co-precipitation process. They studied the process at three different temperatures with a maximum adsorption capacity of  $47.2 \text{ mg g}^{-1}$  at  $35^\circ\text{C}$ . Atrazine removal by natural and  $H_2SO_4$ - and  $NaOH$ -modified bentonite was reported by Ajala *et al.*<sup>35</sup>, giving removal capacities of 76.92, 125.0 and  $111.1 \text{ mg g}^{-1}$ , respectively. Zeolites and activated carbon (C) are the most proven materials, with or without modification, for atrazine removal, but a new generation of materials has increasingly being used for this task. Metal organic frameworks ZIF-8, UiO-66 and UiO-67 were applied by Akpınar *et al.*<sup>36</sup> with capacities of 6.78, 2.57,  $10.96 \text{ mg g}^{-1}$ , respectively. Removal of fluoride and atrazine by magnetic materials also has been reported by Dewage *et al.*<sup>37</sup> and Ali *et al.*<sup>38</sup> In the first case MNP were dispersed on Douglas fir biochar to make a composite for fluoride ion removal using magnetic separation, giving a Langmuir maximum capacity of  $9 \text{ mg g}^{-1}$ . In the second case, an iron nanoparticles composite delivered a maximum adsorption capacity of  $12.2 \mu\text{g g}^{-1}$ .

Many industries use the adsorption process for treating effluents to remove organic and inorganic pollutants,<sup>39</sup> so the demand for low cost and environmental friendly adsorbent materials is evident. Therefore, the purpose of the present research is to study the feasibility of utilizing a SCB magnetic biocomposite (MBo) as a low-cost adsorbent material for fluoride and atrazine removal. Adsorption kinetics were studied, and desorption of iron ions from the composite, during the adsorption process, was analyzed and quantified. This parameter is significant because a high concentration of iron in water could become another environmental pollution problem. MBo were prepared by a co-precipitation



**Figure 1.** Desorption of Fe from  $MB_0$  synthesized by three methods as a function of time (10 mg of  $MB_0$  in 5 mL of water at room temperature, stirred over 24 h).

process to load MNP on the surface of the bagasse. The materials were characterized by Fourier transform infrared (FTIR), scanning and transmission electron microscopy (SEM and TEM), and X-ray diffraction (XRD).

## MATERIALS AND METHODS

### Reagents

The chemical reagents used in this study were analytical grade, were purchased from Sigma-Aldrich, México and used as received.  $NaOH$ ;  $C_2H_5OH$ ;  $NH_4OH$ ,  $FeCl_3 \cdot 6H_2O$  and  $FeCl_2 \cdot 4H_2O$  Atrazine was obtained from SYFATEC S.A. de C.V. (Tlanepantla, México) and was used without further purifications. All necessary dilutions were done with deionized water. The working standard solution of fluoride (Thermo Fisher Scientific) was used for the fluoride adsorption experiments.

### Synthesis of MNP

The MNP were synthesized by the conventional co-precipitation method.<sup>6</sup> In a typical synthesis: 50 mL of  $0.1 \text{ mol L}^{-1}$   $FeCl_3$  and 50 mL of  $0.05 \text{ mol L}^{-1}$   $FeCl_2$  were mixed for 30 min under mechanical stirring in nitrogen atmosphere. Then, 50 mL of  $3.5 \text{ mol L}^{-1}$   $NaOH$  was added drop-wise under stirring and constant inert atmosphere. The color of the reaction changed immediately but was continually stirred for 1 h, until the reaction was completed. Then a black precipitate containing MNP was separated using a magnet. MNP were washed repeatedly with deionized water and dried.

### Preparation of SCB

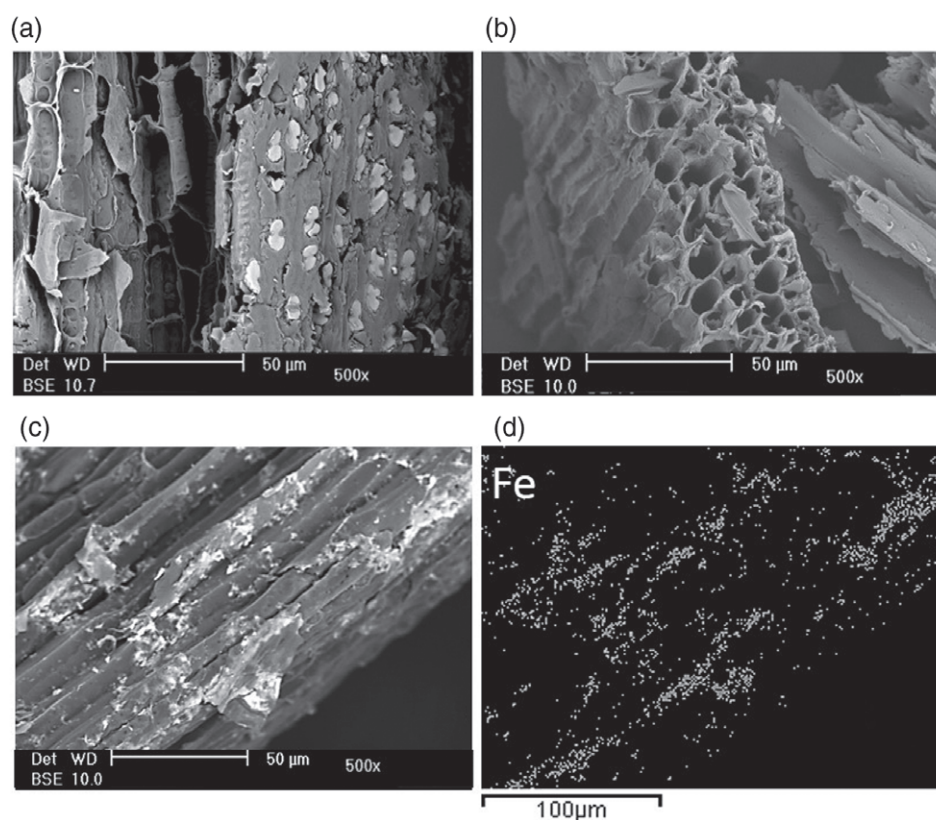
Natural SCB was obtained from a local juice center in Veracruz, Mexico. The material was sun-dried for 5 days, followed by milling and sieving process through  $40\text{--}50 \mu\text{m}$ . The SCB was pretreated in order to avoid possible contaminants, sugars and wax by washing with a  $C_2H_5OH$  solution at 10% v/v for 24 h, at room temperature and magnetic agitation. Then the SCB was filtered and dried before use and labeled as  $B_0$ .

### Magnetic sugarcane bagasse ( $MB_0$ ) preparation

$MB_0$  was synthesized according to three methods:

#### Method I

First, a 50 mL  $FeCl_3$  ( $0.1 \text{ mol L}^{-1}$ ) solution and 50 mL  $FeCl_2$  ( $0.05 \text{ mol L}^{-1}$ ) were mechanically stirred in a nitrogen atmosphere



**Figure 2.** (a) Representative SEM micrographs of natural SCB; (b) treated bagasse  $B_0$ ; (c) magnetic bagasse  $MB_0$ ; and (d) EDS chemical mapping of Fe on the  $MB_0$ , scale bar = 100  $\mu\text{m}$ .

for 30 min. Then, 2 g  $B_0$  was added, the mixture was stirred for another 30 min and the nitrogen atmosphere was maintained. Finally, 50 mL NaOH solution ( $3.5 \text{ mol L}^{-1}$ ) was added drop-wise to the mixture, while maintaining mechanical stirring and nitrogen atmosphere.

#### Method II

First, 50 mL  $\text{FeCl}_3$  ( $0.05 \text{ mol L}^{-1}$ ) solution and 50 mL  $\text{FeCl}_2$  ( $0.025 \text{ mol L}^{-1}$ ) were stirred in a nitrogen atmosphere. Then, 2 g  $B_0$  was added and the mixture was stirred for 30 min. Finally, 50 mL NaOH solution ( $1.75 \text{ mol L}^{-1}$ ) was added drop-wise to the mixture.

#### Method III

First, 50 mL  $\text{FeCl}_3$  ( $0.1 \text{ mol L}^{-1}$ ) solution and 50 mL  $\text{FeCl}_2$  ( $0.05 \text{ mol L}^{-1}$ ) were stirred in a nitrogen atmosphere. Then, 4 g  $B_0$  was added and the mixture was stirred for 30 min. Finally, 50 mL NaOH solution ( $3.5 \text{ mol L}^{-1}$ ) was added drop-wise to the mixture, while maintaining mechanical stirring and nitrogen atmosphere.

In the three methods, the color of bulk solutions changed from orange to black immediately. Mixtures were stirred at  $80^\circ\text{C}$  for 30 min. The  $MB_0$  was washed with distilled water and with EDTA solution ( $0.1 \text{ mol L}^{-1}$ ) to remove the absorbed iron ions, and then with distilled water to neutralize pH.<sup>40</sup> Washed  $MB_0$  was oven-dried at  $50^\circ$  and stored until further use.

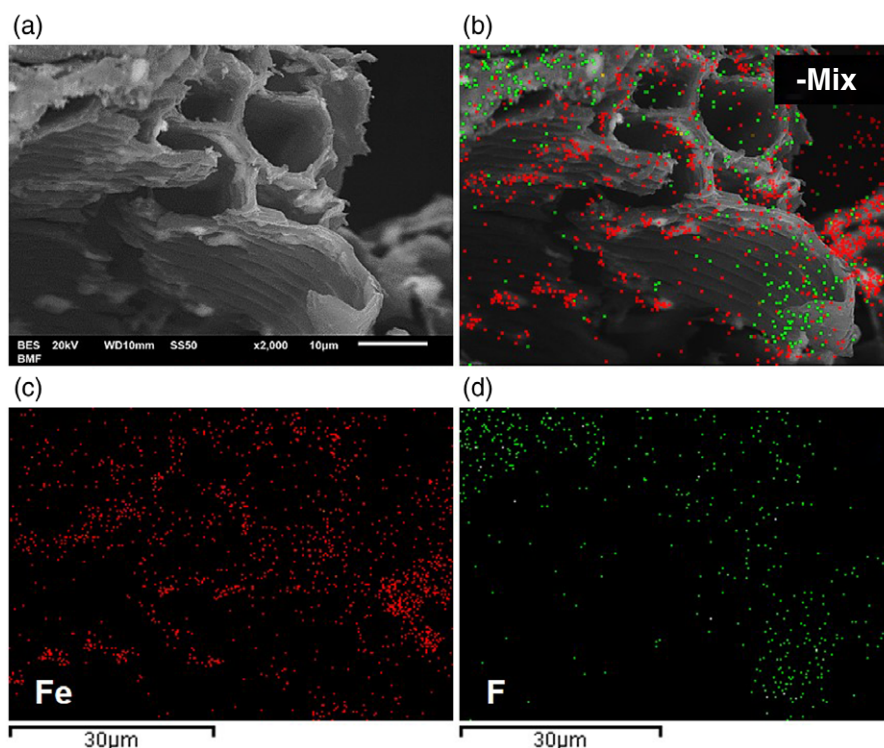
#### Desorption of Fe as a function of time

Desorption experiments of Fe were conducted under static conditions by the batch equilibrium technique, by adding 10 mg  $MB_0$

(synthesized by the three methods mentioned above) to 5 mL deionized water with constant stirring at room temperature. At 0.25, 0.5, 1, 2, 4, 6, 7, 8, 12, 16, 20 and 24 h, the composite  $MB_0$  was isolated with a magnet. Metal content in the suspensions were determined using an atomic absorption spectrometer Philips model PV9100X with a hollow cathode lamp, and a deuterium background corrector using an air-acetylene flame.

#### Characterization

The material phases were identified by XRD analysis performed on a Bruker D8 Advance X-ray diffractometer equipped with a  $\text{CuK}$  radiation source (Karlsruhe, Germany). The nitrogen adsorption-desorption isotherms of the cellulosic support and the composite were determined on an ASAP 2024 Micromeritics device (Georgia, USA), in order to determine the surface area, pore volume and average pore size. A JEOL (Akishima, Japan) microscope model JEM2100 operated at an accelerating voltage of 200 kV with a  $\text{LaB}_6$  filament was used to produce TEM micrographs. The surface morphology was investigated by SEM using a Philips XL-30 (Amsterdam, Netherlands) equipped with a Tungsten gun. In addition, energy-dispersive X-ray spectroscopy (EDX) analyses were carried out in order to obtain chemical composition maps of the different observed sample zones. To elucidate the functional groups present in atrazine, bagasse and the composite after and before the adsorption process, FTIR spectra were recorded in the  $4000$  to  $400 \text{ cm}^{-1}$  region at room temperature by a Bruker (model Tensor-27) FTIR-ATR infrared spectrometer (Ettlingen, Germany). X-ray photoelectron spectroscopy (XPS) wide and narrow spectra were acquired on a JEOL (Akishima, Japan) device model JPS-9200.



**Figure 3.** (a) SEM micrograph of MB<sub>0</sub> after F adsorption; (b) EDS chemical mapping of the Fe and F on the MB<sub>0</sub> after F adsorption, scale bar = 30 μm; (c) and (d) Individual EDS maps showing Fe and F distribution respectively, after the adsorption process.

### Adsorption as a function of time

Adsorption experiments of atrazine were conducted under static conditions by the batch equilibrium technique by adding specified volumes of MB<sub>0</sub> to 5 mL of 30 mg L<sup>-1</sup> pesticide solutions with constant stirring at room temperature. At 0.25, 0.5, 1, 2, 4, 6, 7, 8, 12, 16, 20 and 24 h after contact, MB<sub>0</sub> were separated from the liquid phase (supernatant) by a magnetic field. The pH values of the solutions were between 6.5 and 7.5. The concentrations in the suspensions were determined by a spectrophotometer (UV–visible Perkin Elmer Lambda 10) at 220 nm.

The fluoride kinetic experiments were carried out at a concentration of 3 mg L<sup>-1</sup> with 1 g MB<sub>0</sub> in 200 mL of the solution over a 24 h time interval. The pH values were between 6.8 and 7.09. At certain time intervals, an aliquot of this solution was taken, and the fluoride concentrations were quantified with a selective ion electrode for fluorine, from Thermo Scientific Orion Model 9609BNWP. The ionic strength was controlled with a buffer solution to remove interfering ions.

All data were analyzed using several mathematical kinetic models: pseudo-first-order [Eqn (1)], pseudo-second-order [Eqn (2)] and second-order [Eqn (3)]. The model-fitting and graphics were accomplished using ORIGIN 8.0 software.

$$q_t = q_e (1 - e^{-k_1 t}) \quad (1)$$

$$q_t = \frac{k_2 q_e^2 t}{1 + k_2 q_e t} \quad (2)$$

$$q_t = \frac{1}{\beta} \ln(\alpha\beta) + \frac{1}{\beta} \ln t \quad (3)$$

where  $q_t$  and  $q_e$  (mg g<sup>-1</sup>) are the adsorption capacity of the adsorbent at equilibrium and at time  $t$  theoretical and experimental,

respectively;  $k_1$  (h<sup>-1</sup>) and  $k_2$  (mg g<sup>-1</sup> h<sup>-1</sup>) are the constant rate coefficients for the pseudo-first and pseudo-second order models, respectively; and  $\alpha$  (mg g<sup>-1</sup> h<sup>-1</sup>) and  $\beta$  (g mg<sup>-1</sup>) are the initial adsorption rate, and the activation energy for chemisorption, respectively.<sup>41</sup>

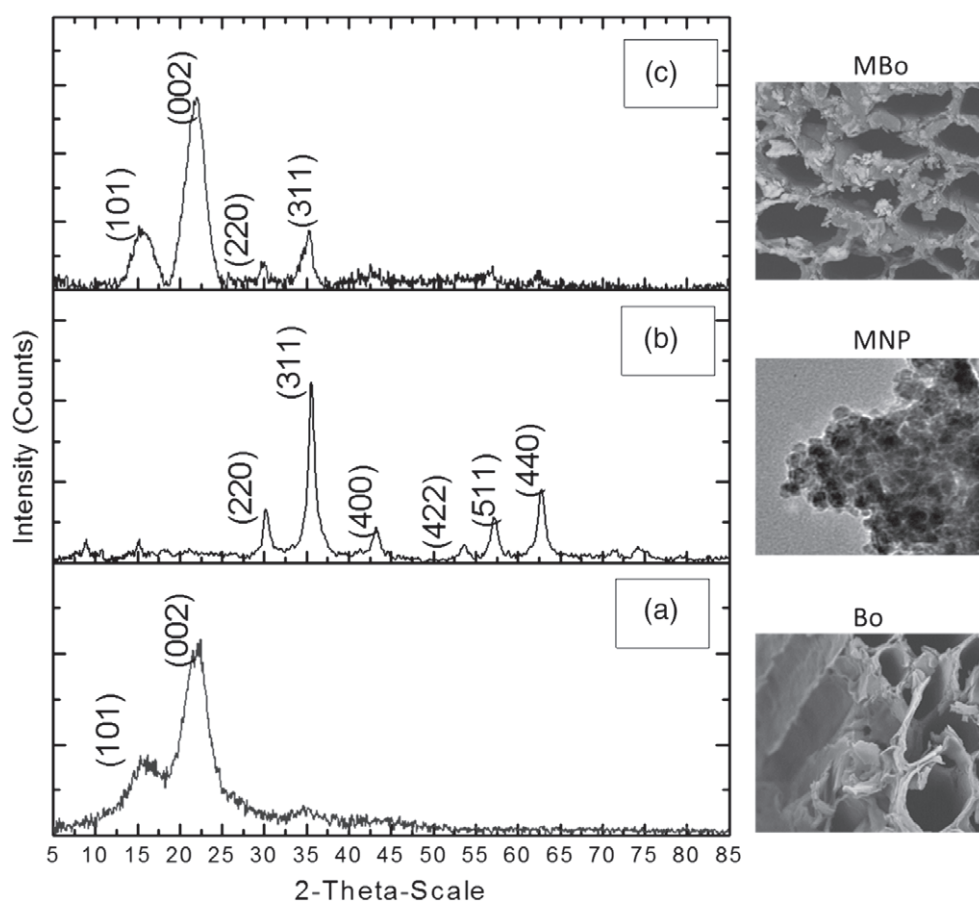
### Adsorption isotherms

The adsorption isotherms of atrazine on MB<sub>0</sub> were determined under the same kinetic conditions. Solutions at different concentrations were prepared, ranging from 10 to 100 mg L<sup>-1</sup>. Afterwards; 5 mL of each solution were individually agitated with MB<sub>0</sub> at the equilibrium time established previously. Next, the mixtures were separated and the solutions were analyzed by a UV-visible spectrophotometer. Fluoride solutions were prepared at a range of concentrations (1–30 mg L<sup>-1</sup>), and 10 mL of each were put in contact with MB<sub>0</sub> materials, and stirred for the equilibrium time at room temperature. Then concentrations of fluoride in the liquids were determined.

The amounts of adsorbed atrazine and fluoride per gram of adsorbent material were calculated and a plot of  $q_e$  as a function of  $C_e$  was built. The experimental equilibrium adsorption data were tested using the two-parameter Freundlich, Langmuir, Temkin and Dubini–Radushkevich isotherm equations, and the three-parameter Langmuir–Freundlich (SIP) equation.

## RESULTS AND DISCUSSION

The three magnetic materials were prepared under the same conditions of temperature, contact time and stirring velocity, and solutions were prepared with the same water and reagents. All conditions were maintained as constant as much as possible. By reducing the concentrations of the reactive solutions from



**Figure 4.** (a) XRD patterns of bagasse (Bo), (b) MNP and (c) MB<sub>0</sub>. The inset of each pattern shows a representative SEM image of Bo, MNP and MB<sub>0</sub>, respectively.

Method I for Method II, we aimed to produce a material with sufficient magnetic response to be removed by a magnetic field after the process while reducing the cost of synthesis. For the same purpose, the concentrations of Method I were kept the same but the mass of SCB for modification was doubled. The color of the resulting MB<sub>0</sub> from methods I and II was black, revealing a higher quantity of nanoparticles than that from Method III. Magnetic response of MB<sub>0</sub> from Method III was not as expected and thus, taking into consideration the desorption of Fe from each material, it was decided to use only the MB<sub>0</sub> from Method I.

#### Desorption of Fe as a function of time

Evaluating the amount of Fe desorbed during the process is important, as the maximum permissible Fe concentration for water discharge to the public sewer system is 25 mg L<sup>-1</sup>.<sup>42</sup> If Fe desorption exceeds this limit, then the process would not be environmentally friendly as Fe would be a new source of water pollution. This also is a significant parameter in case of material regeneration and reuse.

Figure 1 shows desorption of Fe over time from magnetic composites synthesized by three different methods. The Fe concentration in the solutions gradually rose: after 10 h it remained constant for the materials synthesized by methods I and II, whereas equilibrium was achieved at 4 h for material synthesized by Method III. The concentrations at these points were approximately 7.93, 10.4 and 2.20 mg L<sup>-1</sup> for methods I, II and III, respectively.

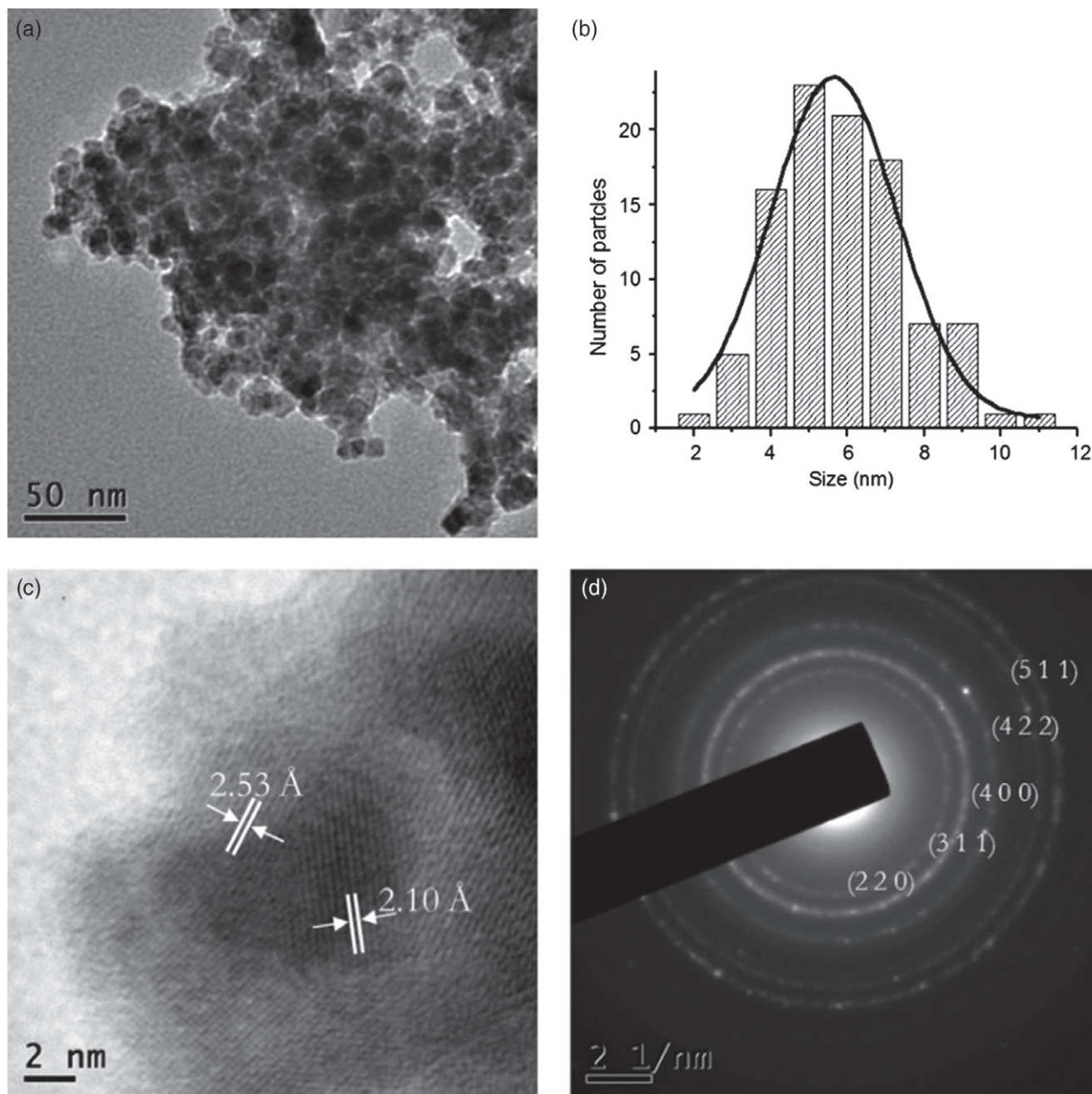
As can be seen, in none of the cases did Fe desorption exceed the allowable limit mentioned above. The material obtained from

method III was discarded as candidate for the adsorption experiments, due to its low magnetic response despite this composite showed the lowest desorption of Fe ions. By doubling the SCB mass in Method III, the amount of supported magnetite decreased so that its low magnetic response did not meet the objective of the synthesis.

Desorption of Fe from material from Method II was higher than that from method I, even though the amount of magnetite supported should be lower as concentrations used were halved. This phenomenon can be attributed to the magnetic characteristics of MNP. When there is a greater number of nanoparticles on the material, they attract each other with greater strength, and desorption of Fe ions decreases. Material synthesized by Method I was thus chosen, based on its visual magnetic response and the analysis of the desorption process. Because it was established that the composite desorbed Fe during the adsorption process, it will be important to perform a more specific study of the material regeneration capabilities as reported for magnetic composites.<sup>43</sup>

#### Material characterization

Figure 2(a) shows the micrograph of the natural SCB. Morphologically, it is a very heterogeneous material with channels and pores of different sizes and shapes; having had no treatment or pre-wash, blocked pores and closed channels can be observed. In Fig. 2(b), channels and pores are unblocked after treatment with C<sub>2</sub>H<sub>5</sub>OH, corresponding to B<sub>0</sub>. Nanomagnetite on the composite MB<sub>0</sub> can be observed outside the channels in Fig. 2(c).



**Figure 5.** (a) Representative TEM micrograph of the MNP, (b) size distribution histogram of MNP, (c) MNP examined under high-resolution TEM, and (d) their electron diffraction pattern (SAED).

Chemical mapping of Fe shows the distribution of magnetite on SCB in Fig. 2(d).

Figure 3(a) shows the micrograph of MB<sub>0</sub> after fluoride adsorption. The composite does not show any significant changes on the surface. The chemical mapping of Fe and fluorine (F) in Fig. 3(b) indicates the distribution of both elements; Fe is represented in red [Fig. 3(c)] and F in green [Fig. 3(d)]. These elements are deposited in different areas on the surface but some interaction between magnetite nanoparticles and fluoride ions are possible, which was confirmed by XPS analysis.

In Fig. 4(a), diffraction peaks at 15.6° and 22.2° are assigned to the reflection from the crystallographic planes (101) and (002) that represent the typical XRD pattern for cellulose or for other

lignocellulosic materials. XRD measurement was used to identify the crystalline structure of magnetite nanoparticles. Figure 4(b) shows characteristic peaks at  $2\theta = 30, 35, 43, 54, 57$  and  $62^\circ$ , corresponding to (2 2 0), (3 1 1), (4 0 0), (4 2 2), (5 1 1) and (4 4 0) Bragg reflections, respectively (JCPDS card no. 19-0629), which can be indexed on the basis of the inverse cubic spinel structure of magnetite. The absence of the characteristic peaks of maghemite [Fe(II)-deficient magnetite], ranging from a  $2\theta$  angle of  $20^\circ$  to  $30^\circ$ , verifies that the main phase corresponds to magnetite.<sup>41</sup> The peaks at  $30$  and  $35^\circ$  were still observed in the prepared composite MB<sub>0</sub> [Fig 4(c)], indicating successful synthesis of magnetite crystals on the SCB surface.

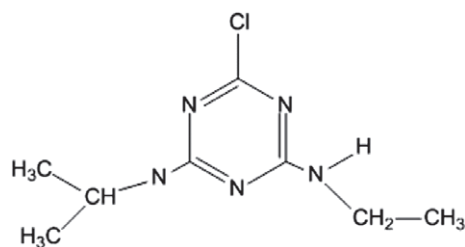


Figure 6. Chemical structure of atrazine.<sup>67</sup>

The Debye–Scherrer equation [Eqn (4)] was used for determining the average crystal particle size of the MNP.<sup>44</sup>

$$D = \frac{K\lambda}{\beta \cos\theta} \quad (4)$$

where  $K$  is a constant related to the Miller index of crystallographic planes (assigned a value of 0.9),  $\lambda$  is the X-ray wavelength,  $\theta$  is half the diffraction angle and  $\beta$  is the angular width (in radians) at half-maximum intensity. MNPs had average diameters of c. 5 nm, which is in agreement with the results of TEM.

The BET surface area of MB<sub>0</sub> was found to be 45.7023 m<sup>2</sup> g<sup>-1</sup> with an average pore width of 63.3 nm, and therefore could be classified as a macroporous material. SEM revealed such porosity in the SCB before and after nanoparticle deposition. The total pore volume was 0.047 cm<sup>3</sup> g<sup>-1</sup> and in general the material is mesoporous, which allows not only the adsorption of small molecules such as fluoride, but also big ones such as atrazine.

A representative TEM micrograph is shown in Fig. 5(a), where semispherical nanoparticles can be seen. They formed agglomerates despite the fact that MNPs were dispersed by ultrasonication. This behavior is due to the magnetic property of the nanoparticles, which attracted each other. This also was associated to desorption of Fe. Small particles with diameters between 2 and 11 nm were identified [Fig. 5(b)]. High-resolution TEM results confirmed the structural nature of the obtained nanoparticles [Fig. 5(c)]. The lattice spaces of 2.1 and 2.53 Å, according to XRD results, correspond to (400) and (311) Bragg reflection, respectively (JCPDS card no. 19-0629). More details were obtained from selected area electron diffraction (SAED) pattern, inset in Fig. 5(d). It also shows the crystalline nature of MNPs, and the typical crystal structure of magnetite, because interplanar distances and diffraction indexes agreed with the standard JCPDS card no. 19-0629.

Atrazine's chemical structure is showed in Fig. 6. The infrared spectra of B<sub>0</sub> is given in Fig. 7(a). The strong signal at 3340 cm<sup>-1</sup> is typical of cellulose<sup>46</sup> hemicellulose and lignin, corresponding to the presence of stretching vibration –OH.<sup>47</sup> Bands at 2913 cm<sup>-1</sup> are characteristic of C–H stretching vibration of methyl groups of lignin. The signal, between 1603 and 1608 cm<sup>-1</sup>, is due to carboxylic groups, present in lignin and hemi-cellulose. Four weak bands around 1450, 1500, 1580 and 1600 cm<sup>-1</sup> represent the C=C vibration in the aromatic rings of lignin. The strong signal at 1039 cm<sup>-1</sup> represents the C–O vibration.

In Fig. 7(b) the spectra of MB<sub>0</sub> is very similar to the spectra of B<sub>0</sub>; however, the signal around 567 cm<sup>-1</sup> is defined more clearly. This band corresponds to the stretching vibrations of Fe–O bonds, which may suggest the presence of magnetite on the surface of the material.<sup>48</sup>

Figure 7(c) presents the spectra of atrazine. The signal at 3253 cm<sup>-1</sup> is for the symmetrical N–H stretching vibration that corresponds to the secondary amine groups of isopropyl and ethyl

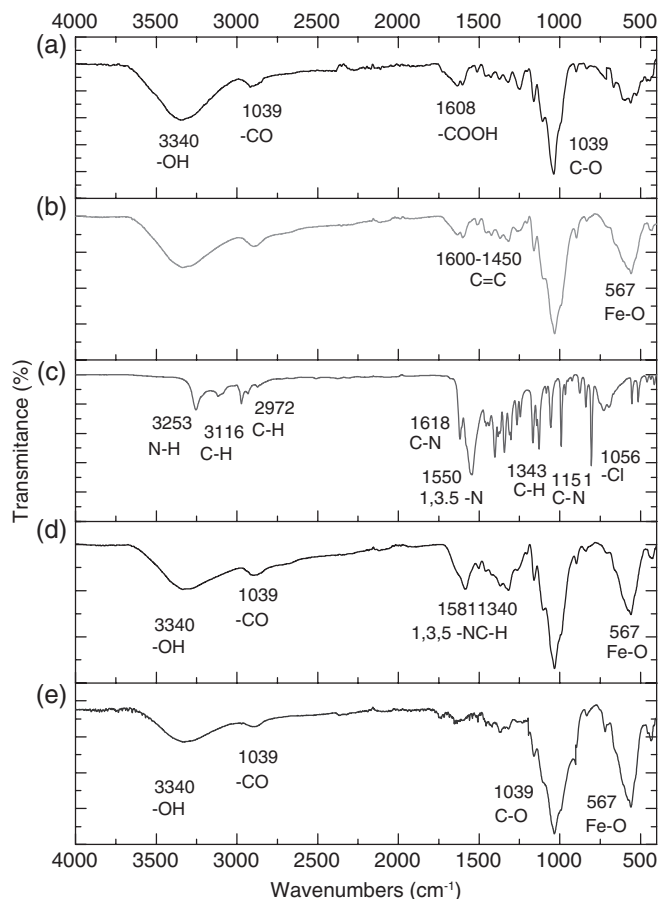
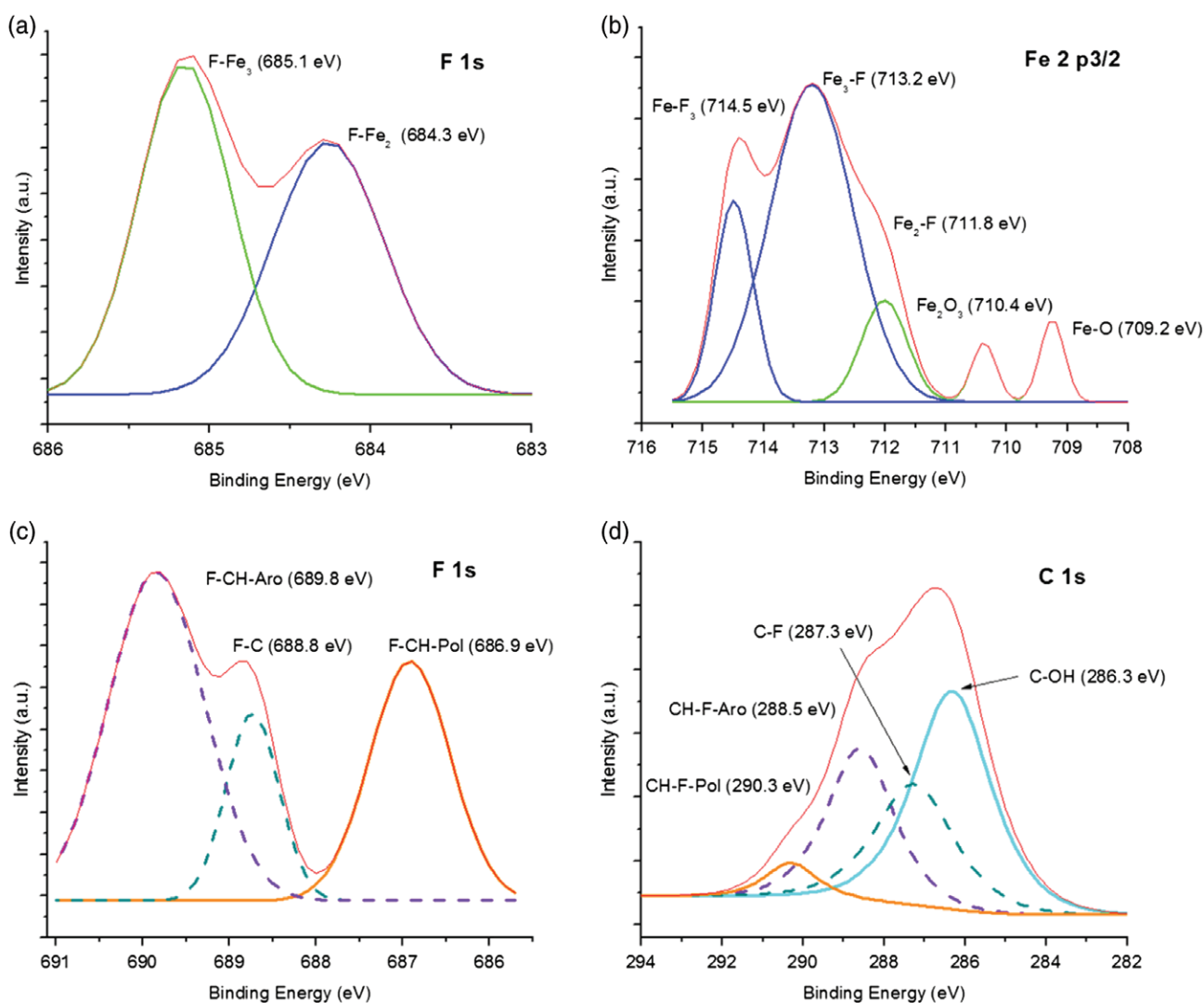


Figure 7. (a) FTIR spectra of bagasse B<sub>0</sub>, (b) MB<sub>0</sub>, (c) atrazine, (d) MB<sub>0</sub> after atrazine adsorption and (e) MB<sub>0</sub> bagasse after fluoride adsorption.

side chain. The stretching vibration C–H linked to the amine in the two branched chains is at 3116 cm<sup>-1</sup>. However, the stretching vibration of C–H corresponding to alkanes is at 2972 cm<sup>-1</sup>.<sup>49</sup> At 1618 cm<sup>-1</sup> it is common to find the stretching vibration of C–N. The strong ring-stretching bands at 1550 and 1410 cm<sup>-1</sup> correspond to three N atoms replacing the 1, 3 and 5 –CH groups in the benzene ring of triazines.<sup>50</sup> At 1343 cm<sup>-1</sup>, the C–H bending vibration of methyl groups can be seen. The stretching vibration for C–N is at 1151 cm<sup>-1</sup>. At 1056 cm<sup>-1</sup> there is a signal related to the aromatic chlorine stretch.

After the adsorption of atrazine in MB<sub>0</sub> a small change can be observed around 1581 and 1540 cm<sup>-1</sup> [Fig. 7(d)]. This slight increase in the signals could be related to the characteristic bands of atrazine. The signals between 2972 and 3253 cm<sup>-1</sup> corresponding to atrazine are overlapped by the most relevant signals of MB<sub>0</sub>. However, not every signal was expected to show up in the spectra because the removal process was established as a chemical adsorption. It means that some changes in the atrazine molecule were expected.

In Fig. 7(e), the MB<sub>0</sub> spectra after the adsorption of fluoride was analyzed. According to Mahapatra *et al.*<sup>51</sup> the signal of C–Cl stretching appears from 850 to 550 cm<sup>-1</sup>. The band in the region 1300–1150 cm<sup>-1</sup> is associated with the symmetrical stretching of –CF group.<sup>52</sup> Therefore, the chemical sorption of this halogen could be identified in this region but the characteristic signals of the composite MB<sub>0</sub> overlap the fluoride signals. However, there are some differences in the intensity and width of the signals



**Figure 8.** XPS spectra of MB<sub>0</sub> after fluoride adsorption: F 1s from 686 to 683 eV (a), F 1s from 691 to 686 eV (c), Fe 2p<sub>3/2</sub> (b), and C 1s (d).

at 1039 and 567 cm<sup>-1</sup> associated with Bo and the Fe–O bond, respectively. They may be attributed to the adsorption of fluoride on the material.

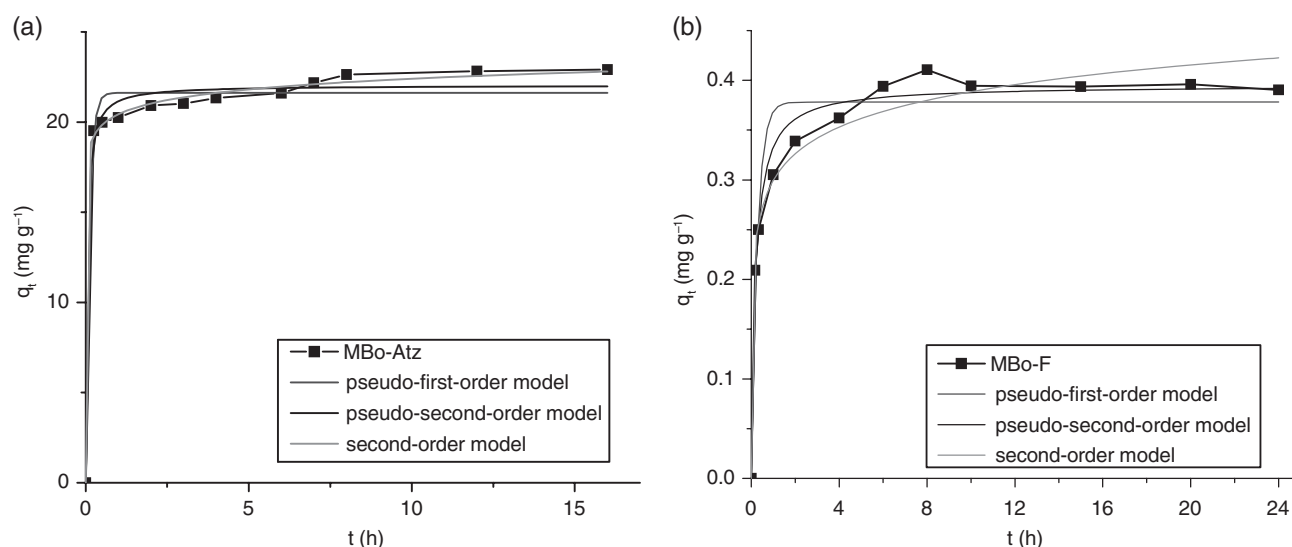
Figure 8 shows XPS spectra of MB<sub>0</sub> after fluoride adsorption; Fig. 8(a) and (b) show the F 1s region, after curve-fitting. Two different chemical environments for fluoride resulted; both signals are related to the interaction between Fe and MNPs. These signals result from an interaction of the analyte with the two different oxidation states of Fe, which was something expected because they form part of the magnetite structure. Interactions of F with C, which is the main component of SCB molecules, are visible in Fig. 8(b). Interactions of polymeric chains (Pol) of –CH, aromatic (Aro) –CH and F–C interactions with lignin and cellulose may take place. In order to confirm the interaction signals, curve-fitting spectra of Fe 2p<sub>3/2</sub>, and C1s are presented in Fig. 8(c) and (d), respectively. In case of Fe 2p<sub>3/2</sub> spectra, not only is the signal related to F present, but also characteristics signals of magnetite. For the C 1s region, there are four signals after curve fitting that can be related to the hydroxyl group (C–OH) from SCB, components such as lignin and cellulose, and also three interactions of F with C, which are in good agreement with the signals observed and discussed before in the F 1s region.

### Adsorption kinetics

The adsorption kinetics of atrazine on MB<sub>0</sub> are illustrated in Fig. 9(a). The adsorption rate in the composite was rapid during the first minutes and equilibrium was achieved at 7 h. The characteristic active sites of the material may have had greater affinity for the pesticide than for the fluoride ions, leading to the high adsorption rate. Atrazine adsorption kinetic parameters of these models are given in Table 1. It can be seen from the statistic values of *R*<sup>2</sup>, RSS and  $\chi^2$  that the adsorption process follows the pseudo-second-order model. The best-fitting models suggest that the present adsorption process is a chemisorption involving valence forces through sharing or exchange of electrons<sup>53</sup> between the composite and atrazine molecules. According to the pseudo-second-order model, the process takes place on a very heterogeneous surface. This result was corroborated with the micrographs of SEM and the spectra of FTIR, where an heterogeneous morphology was observed, and many different kinds of functional groups were established.

For the adsorption of fluoride [Fig. 9(b)], the equilibrium time was 6 h, which is faster than when MB<sub>0</sub> was applied to remove atrazine. This may indicate that as the fluoride molecule is smaller than the atrazine molecule, it can reach the adsorption sites in





**Figure 9.** Adsorption kinetics of atrazine (a) and fluoride (b) onto MB<sub>0</sub> by using mathematical models (10 mg mass in 5 mL of 30 mg L<sup>-1</sup> atrazine, not adjusted pH 6.5–7.5, room temperature; 1 g mass in 200 mL of 3 mg L<sup>-1</sup> of fluoride, not adjusted pH 6.8–7.09, room temperature).

**Table 1.** Kinetic parameters of atrazine and fluoride adsorption by MB<sub>0</sub>

Model <sup>a</sup>	Parameter <sup>b</sup>	Atrazine <sup>c</sup>	Fluoride <sup>c</sup>	Model <sup>a</sup>	Parameter <sup>b</sup>	Atrazine <sup>c</sup>	Fluoride <sup>c</sup>
<b>Pseudo-first-order</b>	$q_e$	21.63	0.3782	<b>Pseudo-second-order</b>	$q_e$	22.04	0.3950
	$k_1$	8.774	3.644		$k_2$	1.083	13.47
	$R^2$	0.9765	0.9339		$R^2$	0.9878	0.9807
	RSS	9.226	$9.470 \times 10^{-3}$		RSS	4.806	$2.760 \times 10^{-3}$
	$\chi^2$	0.9226	$9.468 \times 10^{-4}$		$\chi^2$	0.4806	$2.758 \times 10^{-4}$
<b>Second-order</b>	$\alpha$	2.030	86.29				
	$\beta$	1.169	25.76				
	$R^2$	0.9981	0.9726				
	RSS	0.7416	$3.920 \times 10^{-3}$				
	$\chi^2$	$7.416 \times 10^{-2}$	$3.925 \times 10^{-4}$				

<sup>a</sup> Mathematical models applied to isotherm data.  
<sup>b</sup> Mathematical parameters from models.  
<sup>c</sup> Atrazine removal results from mathematical models.  
<sup>d</sup> Fluoride removal results from mathematical models.  
 $q_e$ , adsorption capacity of the adsorbent at equilibrium time  $t$  (mg g<sup>-1</sup>);  
 $k_1$ , constant rate coefficients for the pseudo-first-order model (h<sup>-1</sup>);  
 $k_2$ , constant rate coefficients for the pseudo-second-order model (g mg<sup>-1</sup> h<sup>-1</sup>).  
 $\alpha$ , initial adsorption rate (mg g<sup>-1</sup> h<sup>-1</sup>).  
 $\beta$ , activation energy for chemisorption (mg g<sup>-1</sup>).

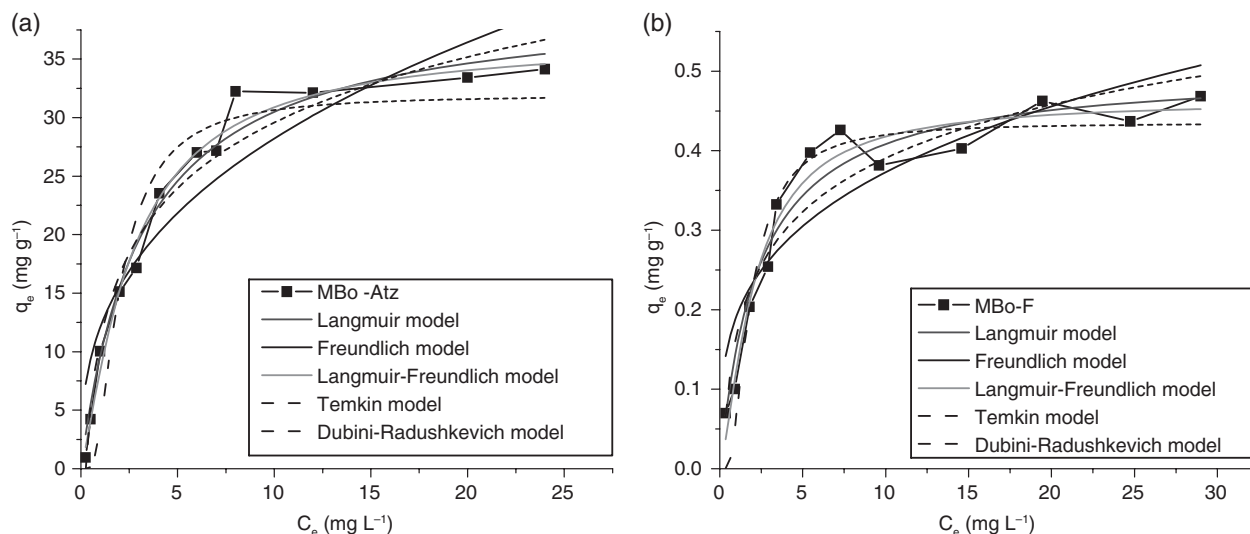
less time. Fluoride spreads faster toward the adsorption sites of the material than atrazine by the size of molecules. After the application of the mathematical models as mentioned above, it was determined that the systems is best described with the pseudo-second-order model (Table 1), pointing out that the adsorption process was a chemisorption.

### Adsorption isotherm

The adsorption isotherms of atrazine and fluoride removal [Fig. 10(a) and (b)] were built at the equilibrium time. Adsorption capacities were established using the model of Langmuir because it is based on the idea of a homogenous monolayer surface phase. The equilibrium factor  $R_L$  calculated with the initial concentration and the Langmuir constant indicates unfavorable adsorption if  $R_L > 1$ , favorable if  $0 < R_L < 1$ , and irreversible if  $R_L = 0$ .<sup>54</sup> The value

for atrazine adsorption is 0.24 and 0.70 for fluoride, and therefore the adsorption is favorable in each case.

The Freundlich model describes an adsorption process in multilayers on heterogeneous surfaces, where interactions of adsorbed molecules can take place.<sup>55</sup> The Sip (Langmuir–Freundlich) isotherm is more suitable to explain the adsorption process on a heterogeneous surface. It predicts the Freundlich isotherm at low adsorbate concentrations, and the monolayer adsorption capacity of the Langmuir isotherm at high concentrations.<sup>56</sup> This model better predicted the adsorption behavior of atrazine and fluoride on MB<sub>0</sub>. Statistics parameters fit better with this model and the characterization of the composite presumes its heterogeneous nature. The Temkin isotherm is an extension of the Langmuir model, which considers variations in the enthalpy of adsorption.<sup>57</sup> Due to adsorbate–adsorbent interactions the energy of the adsorption decreases linearly.<sup>54</sup> The Dubini–Radushkevich model assumes



**Figure 10.** Isotherms of atrazine (a) and fluoride (b) onto MB<sub>0</sub> by using mathematical models (10 mg mass in 5 mL of 10–100 mg L<sup>-1</sup> atrazine, not adjusted pH 6.5–7.5, room temperature; 1 g mass in 200 mL of 1–30 mg L<sup>-1</sup> of fluoride, not adjusted pH 6.8–7.09, room temperature).

**Table 2.** Isotherms parameters of atrazine and fluoride adsorption by MB<sub>0</sub>

Model <sup>a</sup>	Parameter <sup>b</sup>	Atrazine <sup>c</sup>	Fluoride <sup>c</sup>	Model <sup>a</sup>	Parameter <sup>b</sup>	Atrazine <sup>c</sup>	Fluoride <sup>c</sup>
<b>Langmuir</b>	$q_m$	40.11	0.5036	<b>Temkin</b>	A	3.880	5.585
	$K_L$	0.3167	0.4290		B	8.083	$9.710 \times 10^{-2}$
	$R^2$	0.9804	0.9489		$R^2$	0.9665	0.9076
	RSS	26.92	$9.800 \times 10^{-3}$		RSS	45.96	$1.784 \times 10^{-2}$
	$\chi^2$	2.692	$9.876 \times 10^{-4}$		$\chi^2$	4.596	$1.780 \times 10^{-3}$
<b>Langmuir–Freundlich</b>	$q_m$	36.80	0.4638	<b>Dubini–Radushkevich</b>	$q_m$	31.92	0.4351
	$K$	0.2964	0.3666		$B_D$	$7.321 \times 10^{-7}$	$6.362 \times 10^{-7}$
	$1/n$	0.8025	0.7180		E	1.168	1.253
	$R^2$	0.9850	0.9569		$R^2$	0.9240	0.9215
	RSS	18.51	$7.500 \times 10^{-3}$		RSS	104.3	$1.516 \times 10^{-2}$
<b>Freundlich</b>	$\chi^2$	2.057	$8.332 \times 10^{-4}$	$\chi^2$	10.43	$1.520 \times 10^{-3}$	
	$1/n$	0.3690	0.2894				
	$K_F$	12.06	0.1915				
	$R^2$	0.8717	0.8165				
	RSS	176.0	$3.544 \times 10^{-2}$				
	$\chi^2$	17.60	$3.540 \times 10^{-3}$				

<sup>a</sup> Mathematical models applied to isotherm data;

<sup>b</sup> Mathematical parameters from models.

<sup>c</sup> Atrazine removal results from mathematical models.

<sup>d</sup> Fluoride removal results from mathematical models.

$q_m$ , maximum adsorption capacity (mg g<sup>-1</sup>).

$K_L, K, K_F$ : Langmuir, Langmuir–Freundlich, Freundlich constants (L mg<sup>-1</sup>).

$1/n$ , adsorption intensity constant.

A, Temkin binding constant.

B, heat of adsorption (J mol<sup>-1</sup>).

$B_D$ , Dubinin–Radushkevich isotherm constant (mol<sup>2</sup> J<sup>-2</sup>).

E, adsorption energy (kJ mol<sup>-1</sup>).

$R^2$ , Correlation coefficient.

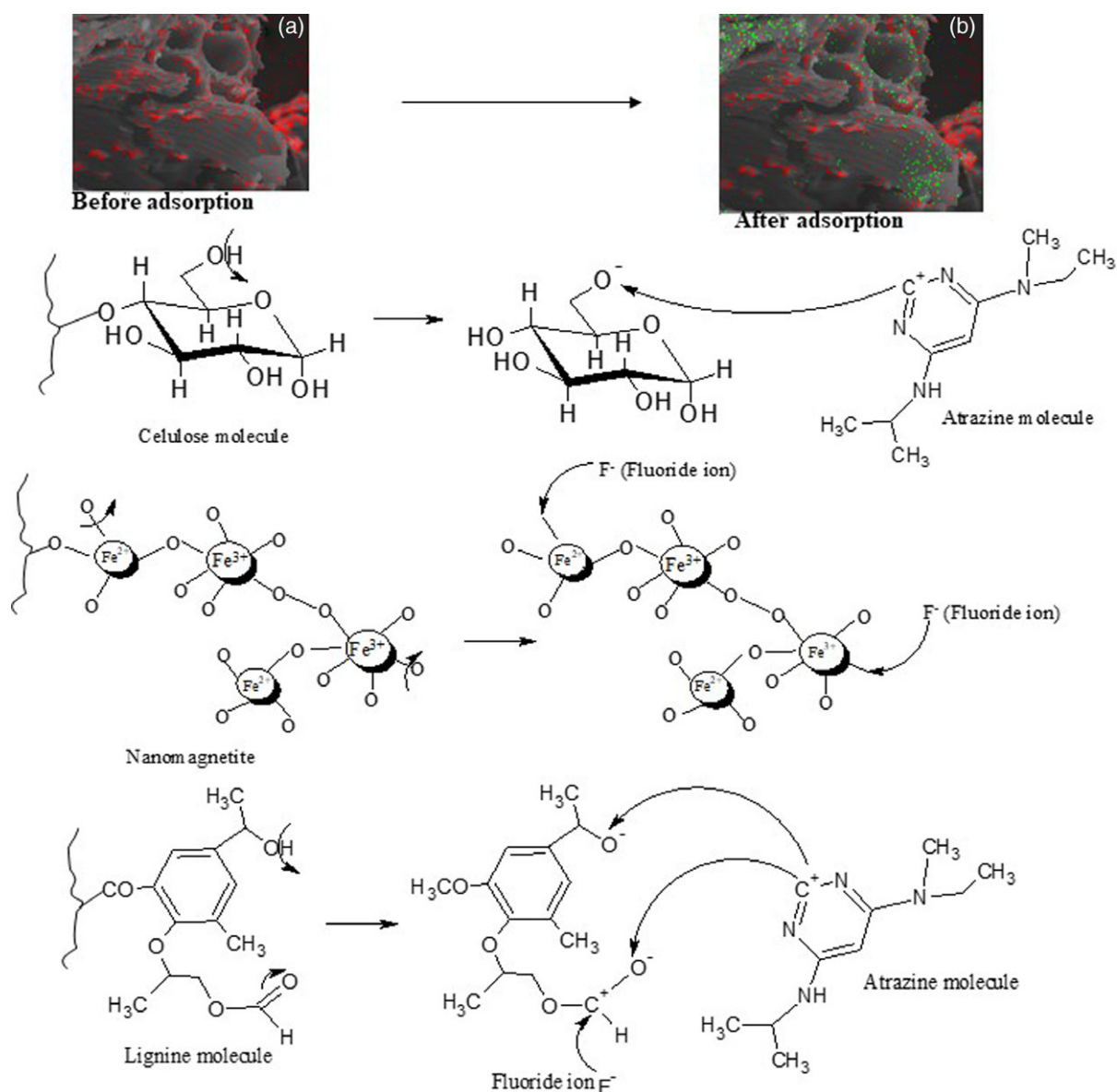
RSS, residual sum of squares.

$\chi^2$ , reduced chi-square.

that the adsorption mechanism is carried out with a Gaussian distribution of energy over an heterogeneous surface. It is applied to distinguish between a chemisorption and a physisorption.<sup>58</sup>

Calculated parameters for Langmuir, Freundlich, Langmuir–Freundlich, Temkin and Dubini–Radushkevich models are given in Table 2. The best-fitting model for the removal of atrazine onto MB<sub>0</sub> was Langmuir–Freundlich. This model is a versatile

isotherm expression that can simulate both Langmuir and Freundlich behaviors.<sup>59</sup> The dimensionless heterogeneity factor  $1/n$  describes the heterogeneity of the material because  $0.8025$  is between 0 and 1. The value of  $1/n < 1$  is related to the adsorption intensity constant that varies with the heterogeneity of the adsorbate.<sup>60</sup> The adsorptive capacity was  $40.11 \text{ mg g}^{-1}$  for the removal of atrazine onto MB<sub>0</sub>. There are no previous reports of



**Figure 11.** Scheme for the adsorption mechanism of atrazine and fluoride by  $MB_0$ . Inserts a and b correspond to EDS chemical mapping of  $MB_0$  before and after the F adsorption, respectively.

the removal of atrazine with this kind of composite; however, with another magnetic composite Castro *et al.* reported a  $q_{max}$  of  $25 \text{ mg g}^{-1}$ .<sup>61</sup> They reported that the atrazine adsorption capacity diminishes as the content of Fe in the composites increases, maybe because the impregnation with Fe oxide reduced the surface area by its deposition in the activated C pores. In our case, as can be seen in the characterization of the material, the magnetite does not block the pores of the bagasse.

According to Table 2, the best adjusted to the experimental data obtained for  $MB_0$  in the adsorption of fluoride was for the Langmuir–Freundlich model. Therefore, the adsorption took place through a heterogeneous surface and the dimensionless heterogeneity factors  $1/n$  are between 0 and 1 (0.7180). The Langmuir adsorption model has been broadly used to estimate the adsorption capacity of several elements and chemical species.<sup>62</sup> This allowed establishing a capacity of  $0.5036 \text{ mg g}^{-1}$ .

In comparison to other research, the fluoride adsorption capacity of  $MB_0$  obtained herein is low. Dhillon *et al.*<sup>63</sup> determined

an adsorption capacity of  $194 \text{ mg g}^{-1}$  for a novel Ce–Zn binary metal oxide adsorbent and Wu *et al.*<sup>64</sup> reported  $32.310 \text{ mg g}^{-1}$  when using a hybrid adsorbent fabricated with Mg/Fe composite oxide and alginate. A more similar material to that explored in the present paper was tested by Jayarathna.<sup>32</sup> They synthesized nanoparticles of maghemite by the co-precipitation method and found that the fluoride removal capacity was  $3.65 \text{ mg g}^{-1}$ , and that it strongly depended on initial pH of solutions. Singh *et al.*<sup>21</sup> reported that, SCB removed fluoride from aqueous solution with a maximum adsorption capacity of  $4.12 \text{ mg g}^{-1}$ . According to this reference, and fluoride adsorption results in the present work, MNP diminishes the adsorption capacity of the support material, which can be attributed to the fact that the nanoparticles would be occupying active sites. Therefore, the tested materials may only be applied as adsorbent materials for low concentrations of fluoride. In order to understand this behavior a more detailed study is planned in a forthcoming work.

The atrazine removal capacity of MB<sub>0</sub> is higher than data reported for other adsorbent materials including activated peanut husk (4.11 mg g<sup>-1</sup>)<sup>31</sup> and biochars produced from soya beans (1.38 mg g<sup>-1</sup>).<sup>65</sup> However, Lladó *et al.*<sup>66</sup> determined the adsorption capacity of three different activated Cs, two of them commercial with higher adsorption capacity (212.26 and 119.45 mg g<sup>-1</sup>). Nevertheless, the third was a sludge-based activated C with an adsorption capacity of 45.49 mg g<sup>-1</sup>, similar to the MB<sub>0</sub> composite.

According to results obtained from mathematical models of kinetics and isotherms of adsorption, as well as the identification of functional groups of the material characterization by FTIR and chemical environment of F from XPS results, a mechanism of adsorption for F and atrazine was proposed (Fig. 11).

The composite has a greater affinity with atrazine than with fluoride. Perhaps to improve the removal of fluoride other elements should be incorporated to the composite to increase fluoride affinity.

## CONCLUSIONS

Magnetite is a well-known mineral whose magnetic properties render its efficiency in adsorption processes, because it would facilitate its separation from the system once used for contaminant removal. The affinity of the MB<sub>0</sub> composite towards atrazine is greater than with fluoride. The equilibrium times are related to the rate constants in each best-fitted model. Both processes of adsorption were carried out by a chemisorption, which means that the adsorbate removed would be confined within the composite. The adsorption capacities varied, but the highest was obtained for the composite MB<sub>0</sub> and the removal of the pesticide. The adsorption capacity to remove fluoride was < 1 mg g<sup>-1</sup>. However, its characteristics would allow the material to be used for fluoride removal in water containing low concentrations of this contaminant.

The synthesis of the magnetic composite is simple, facilitating mass production, and generates a material easy to manipulate and easy to isolate after the process. It is a novel material that has not yet been tested for the removal of these types of contaminants. As Fe desorption during the adsorption process did not exceed the maximum permissible concentration for water discharge, the composite MB<sub>0</sub> can be considered to be environmentally friendly and important adsorbent material in larger scale processes.

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