

# GASES IDEALES Y REALES

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## Gases ideales y Factor de Compresibilidad

## Datos / Modelos Gases Reales

## Carta Básica Compresibilidad

**Ideales**  
 Si  $P \rightarrow 0 \Rightarrow \frac{PV}{T} \rightarrow R$   
 Si  $T \uparrow \Rightarrow$  Ideal  
 Si  $P \uparrow \Rightarrow$  Real

**Ideal**  
 Traducción azarosa de las moléculas.  
 Moléculas con volumen nulo  
 Moléculas sin atracción entre sí  
 Gases en su mayoría son diatómicos:  $N_2$ ,  $O_2$ ,  $Cl_2$ ,  $F_2$   
 Gases triatómicos:  $O_3$   
 Gases moleculares:  $CO_2$ ,  $CH_4$ ,  $NO_x$ ,  $SO_x$

**Real**  
 Considera tamaño de partículas  
 Interacción de las partículas  
 Estados fuera de equilibrio  
 Disociación molecular  
 Puede considerar reacciones

$$PV = nRT$$

$$P = \frac{n}{V} \cdot N_A \cdot \frac{RT}{N_A}$$

$$P = NkT$$

$N = \# \text{total moléculas} / \text{unidad volumen}$

**Van der Waals**

$$\left[ P + a \left( \frac{n}{V} \right)^2 \right] (V - nb) = nRT$$

$$a = \frac{27(RT_c)^2}{64P_c}, \quad b = \frac{RT_c}{8P_c}$$

**Boyle (isotermas)**  
 $V \propto \frac{1}{P} \quad VP = cte$

**Charles (Ley expansión) (isobaras)**  
 $V \propto T \quad \frac{V}{T} = cte$

**Gay-Lussac (isocoras)**  
 $P \propto T \quad \frac{P}{T} = cte$

**Avogadro (isopletras)\***  
 $V \propto n$

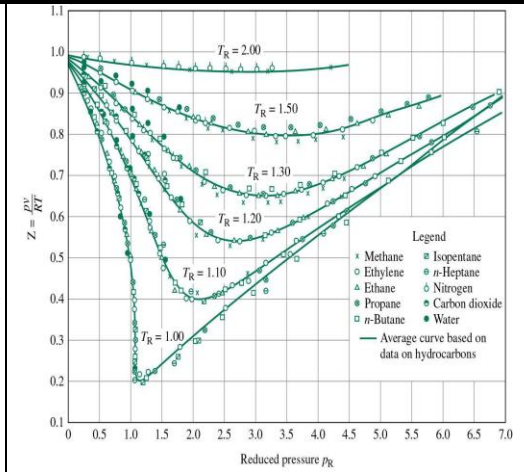
\* Composición constante

**Valores R:**  
 atm L / (mol K): 0.08206  
 atm cm<sup>3</sup> / (mol K): 82.0575  
 J / (mol K): 8.314462  
 kPa m<sup>3</sup> / (kmol.K): 8.314462  
 psi pie<sup>3</sup> / (lbmol °R): 10.73  
 bar L / (mol K): 0.08314472  
 Btu / (lbmol °R): 1.9859  
 (kg/cm<sup>2</sup>) L / (mol K): 0.0847  
 mmHg / (mol K): 62.364  
 plgHg pie<sup>3</sup> / (lbmol °R) 21.85

°C = (°F - 32) ÷ 1.8  
 °F = (°C × 1.8) + 32  
 °C = K - 273.15  
 °R = °F + 459.67

$R_{\text{aire}} = 0.287 \text{ kJ} / (\text{kg K})$   
 $R_{\text{bióxido carbono}} = 0.187$   
 $R_{\text{nitrógeno}} = 0.2968$   
 Volumen molar ( $V_m$ ) = 22.414 L STP  
**IUPAC (STP) NIST, ISO, EEA, ICAO:**  
 273 K, 1atm  
 Número Avogadro ( $N_A$ ):  
 $6.02214129 \times 10^{23}$   
 Constante Boltzmann (k)  
 $k = \frac{R}{N_A}$   
 $1.3806504(24) \times 10^{-23} \text{ J K}^{-1}$   
 $8.617343(15) \times 10^{-5} \text{ eV K}^{-1}$   
 $0.00831447 \text{ kJmol}^{-1}\text{K}^{-1}$

1 atm = 760 mmHg = 760 torr =  
 1.01325 bar = 14.696 psi = 0.7037 at  
 1cm H<sub>2</sub>O = 98.064 Pa @ 4°C



**Factor Compresibilidad (Z)**

$$PV = ZnRT$$

Para mayoría de gases  
 $Z_c = 0.2 - 0.33$   
 $P_r = \frac{P}{P_c}, \quad T_r = \frac{T}{T_c}, \quad V_r = \frac{V \cdot P_c}{R \cdot T_c}$   $r = \text{reducido}, \quad c = \text{crítico}$

**Redlich-Kwong**  
 $\bar{v} = \text{volumen molar} \quad (m^3 / \text{mol})$

$$P = \frac{RT}{\bar{v} - b} - \frac{a}{\sqrt{T}\bar{v}(\bar{v} + b)} \quad a = \frac{0.42748R^2T_c^{2.5}}{P_c} \quad b = \frac{0.08662RT_c}{P_c}$$

Fórmula	Constantes Críticas				Acéntrico	Coeficientes de Van der Waals	
	T <sub>c</sub> (K)	P <sub>c</sub> (MPa)	10 <sup>6</sup> V <sub>c</sub> (m <sup>3</sup> /mol)	Z <sub>c</sub>		10 <sup>3</sup> a (m <sup>6</sup> Pa/mol <sup>2</sup> )	10 <sup>6</sup> b (m <sup>3</sup> /mol)
He	5.3	0.229	61.6	0.29	0	3.45	23.7
H <sub>2</sub>	3.33	1.30	69.7			24.7	26.6
N <sub>2</sub>	126.1	3.39	90.0	0.291	0.040	141	39.1
CO	134.0	3.51	90.0	0.294	0.046	151	39.9
O <sub>2</sub>	154.3	5.04	74.4			138	31.8
C <sub>2</sub> H <sub>4</sub>	282.9	5.16	127.5	0.270	0.087	453	57.1
CO <sub>2</sub>	304.2	7.38	94.2	0.274	0.420	365	42.7
NH <sub>3</sub>	405.6	11.37	72.0	0.242	0.252	422	37.1
H <sub>2</sub> O	647.2	22.06	55.44			553	30.5
Hg	1735.0	105.0	40.1			820	17.0

**Dieterici**

$$P = \frac{nRT}{V - nb} e^{-\frac{na}{VRT}} \quad a = \frac{RT_c}{e^2 P_c}, \quad b = \frac{4R^2 T_c^2}{e^2 P_c}$$

**Berthelot**

$$P = \frac{nRT}{V - nb} - \frac{n^2 a}{TV^2} \quad a = \frac{27R^2 T_c^3}{64P_c}, \quad b = \frac{RT_c}{8P_c}$$

**Beattie-Bridgeman**  
 $P \leq 0.8P_c$

$$P = \frac{R_u T}{\bar{v}} \left( 1 - \frac{c}{\bar{v} T^3} \right) (\bar{v} + B) - \frac{A}{\bar{v}^2}$$

$R_u$  y  $\bar{v}$  son referidas a mol<sup>-1</sup>  
 $A = A_0 \left( 1 - \frac{a}{\bar{v}} \right)$  y  $B = B_0 \left( 1 - \frac{b}{\bar{v}} \right)$

**Benedict-Webb-Rubin**  
 $P \leq 2.5P_c$

$$P = \frac{R_u T}{\bar{v}} + \left( B_0 R_u T - A_0 - \frac{C_0}{T^2} \right) \frac{1}{\bar{v}^2} + \frac{b R_u T - a}{\bar{v}^3} + \frac{a\alpha}{\bar{v}^6} + \frac{c}{\bar{v}^3 T^2} \left( 1 + \frac{\gamma}{\bar{v}^2} \right) e^{-\frac{\gamma}{\bar{v}^2}}$$

**Peng-Robinson**  
 $\omega = -\log_{10}(P_r^{sat}) - 1$   
 @  $T_r = 0.7$

$$P = \frac{RT}{\bar{v} - b} - \frac{a\alpha}{\bar{v}^2 + 2b\bar{v} - b^2} \quad a = \frac{0.45724R^2 T_c^2}{P_c} \quad b = \frac{0.07780RT_c}{P_c}$$

$\alpha = (1 + (0.37464 + 1.54226\omega - 0.26992\omega^2)(1 - T_r^{0.5}))^2$ ;  $\omega = \text{factor acéntrico}$

**Ecuación Virial**

$$\frac{P\bar{v}}{RT} = 1 + \frac{B}{\bar{v}} + \frac{C}{\bar{v}^2} + \frac{D}{\bar{v}^3} + \dots; \quad B = -V_c; \quad C = \frac{V_c^2}{3}$$

T es Temperatura de Boyle  
 Cuando B = 0